
Model for Mixed- Suspension-Mixed Product Removal Crystallizer

Average particle size and nucleation rate.

- Further derivation of the population approach results in the equation for the average size L_a in mm of the mass distribution:

$$L_a = 3.67 G \tau \quad (25)$$

- Here, 50% of the mass of the product is smaller or larger in size than this value. Also, the predominant particle size is given as

$$L_d = 3.00 G \tau \quad (26)$$

- This predominant particle size means more of the mass is in this differential size interval than in any other size interval.
- Another relation can be obtained from this model, which relates the nucleation rate B° to the value of the zero-size particle population density n° and the growth rate G .
- For the condition $L \rightarrow 0$, the limit of dN/dt (nucleation rate) can be written as

$$\lim_{L \rightarrow 0} \frac{dN}{dt} = \lim_{L \rightarrow 0} \frac{dN}{dL} \frac{dL}{dt} \quad (27)$$

- However, when $L \rightarrow 0$, the slope $dL/dt = G$, the slope $dN/dL = n^\circ$, and $B^\circ = dN/dt$. Hence,

$$B^\circ = G n^\circ \quad (28) \quad B^\circ = \text{nucleation rate in number of nuclei/h} \cdot L$$



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